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<b>(21) International Application Number:</b> PCT/GB98/01019 <b>(22) International Filing Date:</b> 7 April 1998 (07.04.98) <b>(30) Priority Data:</b> 9707880.2 18 April 1997 (18.04.97) GB <b>(63) Related by Continuation (CON) or Continuation-in-Part (CIP) to Earlier Application</b> US 60/044,409 (CIP) Filed on 29 April 1997 (29.04.97) <b>(71) Applicant (for all designated States except US):</b> NYCOMED IMAGING AS [NO/NO]; Nycoveien 1-2, N-0401 Oslo (NO). <b>(71) Applicant (for GB only):</b> COCKBAIN, Julian [GB/GB]; 27 Ladbroke Road, London W11 3PD (GB). <b>(72) Inventors; and</b> <b>(75) Inventors/Applicants (for US only):</b> HOMESTAD, Ole, Magne [NO/NO]; Nycomed Imaging as, Nycoveien 1-2, N-0401 Oslo (NO). MYRBRÅTEN, Espen [NO/NO]; Nycomed Imaging AS, Nycoveien 1-2, N-0401 Oslo (NO).		<b>(74) Agents:</b> COCKBAIN, Julian et al.; Frank B. Dehn & Co., 179 Queen Victoria Street, London EC4V 4EL (GB).  <b>(81) Designated States:</b> AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GE, GH, GM, GW, HU, ID, IL, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, US, UZ, VN, YU, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG).  <b>Published</b> <i>With international search report.</i> <i>Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>
<b>(54) Title:</b> CONTRAST AGENT PREPARATION  <b>(57) Abstract</b>  In the metallation of complexing agents such as DTPA-BMA with a lanthanide using a lanthanide oxide such as the lanthanide source, oxalic acid is used as a reaction accelerator.		

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### Contrast Agent Preparation

This invention relates to a process for the metallation of complexing agents with lanthanides, e.g. gadolinium, and in particular to the preparation of lanthanide chelates such as those suitable for use as contrast agents in diagnostic imaging modalities such as magnetic resonance (MR) imaging.

In MR imaging, the use of lanthanide chelates as contrast agents has become well established. Several such agents (eg. Gd DTPA, Gd DTPA-BMA and Gd HP-D03A, available under the trade marks Magnevist, Omniscan and Pro-Hance) are already commercially available, while still others are in early, middle and late stages of development. Such contrast agents are complexes of lanthanide ions with various different complexing agents (ligands) and a key stage of their production is the metallation of the ligand with a lanthanide. In general this is the last stage of primary production, ie. the production of the chemical drug substance that is subsequently formulated into the drug product in the secondary production phase.

Between metallation and secondary production the lanthanide complex must be thoroughly purified to remove unwanted impurities. As with any commercial drug synthesis, it is important to optimize yield of the desired product, reduce the levels of impurities produced during the various synthetic steps, and reduce process duration (and so optimize the efficiency of reactor usage).

Metallation with lanthanides is normally performed by reacting the ligand with a lanthanide oxide (e.g.  $Gd_2O_3$ ) in a heated aqueous medium. If this reaction takes too long, decomposition of the ligand can occur, resulting in reduction in yield and increased levels of impurities in the end product.

Thus for example in the metallation of DTPA-BMA (diethylene-triaminepentaacetic acid-N,N'-bis(methylamide) with gadolinium oxide, where the metallation proceeds too slowly some breakdown of the ligand to the mono-methylamide DTPA-MMA occurs. The reaction product then includes both Gd DTPA-BMA and a salt, eg. the sodium salt, of Gd DTPA-MMA. As a result NaGd DTPA-MMA must be removed by a recrystallization procedure.

The lanthanide oxide used in the metallation process is produced commercially by thermal decomposition of a lanthanide oxalate.

It has now surprisingly been found that the rate of the ligand metallation reaction is increased if the reaction medium includes oxalic acid or derivatives (eg. salts thereof).

Thus viewed from one aspect the invention provides a process for the preparation of a lanthanide complex by reaction of a lanthanide oxide with a complexing agent in an aqueous reaction medium, characterised in that oxalic acid or a salt or derivative thereof is used as a reaction accelerator.

When the ligand is subject to thermal decay, the process of the invention will represent an improvement in terms of speed of reaction as well as reduction in by-product formation; however, even where the ligand is thermally stable an improvement in speed of reaction will still be achieved.

The lanthanide used according to the invention may be any lanthanide but preferably is Eu, Tb, Tm, Yb, Er or Ho, more preferably Dy, and most preferably Gd.

In this process where oxalic acid or a salt or derivative thereof is used as a reaction accelerator, this relates to further oxalic acid and not simply to the oxalate residue in the lanthanide oxide, even though this residue will of course contribute to the acceleration of the reaction.

The total amount of oxalic acid (or salt or

derivative) added as a reaction accelerator is conveniently at least 10  $\mu\text{g}$  oxalic acid/g  $\text{L}_2\text{O}_3$  (where L is the lanthanide, e.g. Gd), preferably at least 50  $\mu\text{g}/\text{g}$ , especially at least 100  $\mu\text{g}/\text{g}$ , particularly at least 200  $\mu\text{g}/\text{g}$  and more particularly at least 400  $\mu\text{g}/\text{g}$ , eg. about 500  $\mu\text{g}/\text{g}$ . The amount added will preferably be less than 2000  $\mu\text{g}/\text{g}$ , particularly less than 1000  $\mu\text{g}/\text{g}$ , preferably less than 800  $\mu\text{g}/\text{g}$ .

The oxalic acid reaction accelerator can be added to the metallation reaction mixture as a separate reagent. However in alternative aspects of the invention some or all of the oxalic acid/oxalate may derive from oxalate impurity in the lanthanide oxide.

Thus viewed from a further aspect the invention provides a process for the preparation of a lanthanide complex by reaction of lanthanide oxide with a complexing agent in an aqueous reaction medium, characterised in that said process comprises the steps of: (a) determining the level of impurity in the lanthanide oxide; and (b) mixing lanthanide oxide from batches with different determined levels of impurity and/or including in the reaction medium a predetermined quantity of oxalic acid or a salt or derivative thereof; whereby by virtue of step (b) the reagents used in the metallation reaction contain oxalic acid (or salt or derivative) or oxalate at a total level of at least 50  $\mu\text{g}$  oxalic acid per gram  $\text{L}_2\text{O}_3$ , preferably at least 100  $\mu\text{g}/\text{g}$ , more preferably at least 200  $\mu\text{g}/\text{g}$ , especially at least 250  $\mu\text{g}/\text{g}$  and particularly preferably at least 400  $\mu\text{g}/\text{g}$ , eg. up to 1750  $\mu\text{g}/\text{g}$ , particularly 700 to 900  $\mu\text{g}/\text{g}$ .

Viewed from a yet further aspect the invention provides a process for the preparation of a lanthanide complex by reaction of a lanthanide oxide with a complexing agent in an aqueous reaction medium, characterised in that for use as said lanthanide oxide is selected a lanthanide oxide having (eg. pre-analysed to contain) an oxalate impurity level of at least 100  $\mu\text{g}$  oxalic acid/g lanthanide oxide, preferably at least 200

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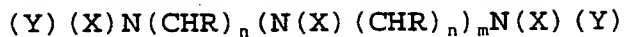
$\mu\text{g/}$ , more preferably at least 250  $\mu\text{g/g}$ , especially preferably at least 400  $\mu\text{g/g}$ , more especially at least 700  $\mu\text{g/g}$ .

The oxalate impurity level of the  $\text{L}_2\text{O}_3$  may be inferred from its residue on ignition - the higher the residue the higher the oxalate content. Alternatively it can be determined by suitable analytical methods.

Where oxalic acid is added to the reaction medium, with or without predetermination of oxalate impurity levels of the lanthanide oxide, it may be added as a salt (eg. an alkali metal or alkaline earth metal salt), an ester or an amide or as the free acid. Lanthanide oxalates themselves may be used. However, preferably the free acids are used.

The use of oxalic acid (or salts or derivatives thereof) can reduce the metallation reaction time by a factor of two or more, eg. by a factor of up to 6.

The ligand which is metallated may be any ligand capable of producing a highly stable lanthanide complex, eg. one with a dissociation constant of at least  $10^{12}$ . Preferably it will be a linear, cyclic or branched chelating agent, eg. a linear mono- or polychelant, a macrocyclic chelant or a branched polychelant (eg. a dendrimeric polychelant). Preferably the ligand will be a polyaminopolyoxyacid (eg. polyaminopolycarboxylic acid), such as one of the mono and polychelants suggested for lanthanide chelation in the patent literature relating to MR contrast agents, eg. the patent publications of Nycomed (including Nycomed Imaging and Nycomed Salutar), Sterling Winthrop, Schering, Bracco, Squibb, Mallinckrodt, Guerbet and Metasyn, eg. US-A-4647447, EP-A-71564, WO96/03154, WO96/01655, EP-A-430863, WO96/41830, and WO93/10824. Thus by way of example the ligand may be of formula



where  $m$  is 0, 1, 2, or 3;  
 $n$  is 2 or 3;

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each X is a hydrogen or a substituted  $C_{1-6}$  alkyl group;  
each Y is a group X or the two Y groups together  
represent a  $(CHR)_n$  bridge;  
and each R is hydrogen or a substituted  $C_{1-6}$  alkyl group  
or a  $CHR-N(X)-CHR$  moiety may represent an optionally  
substituted, saturated or unsaturated 5 to 7 membered  
heterocyclic ring or a  $CHRCHR$  moiety may represent an  
optionally substituted, saturated or unsaturated 5 to 7  
membered homo- or heterocyclic ring;  
where at least two X groups are alkyl groups substituted  
by sulphur, phosphorus or carbon oxyacid groups or  
amides or esters thereof, and where alkyl group  
substitution is preferably by oxyacid or oxyacid  
derivative groups, by hydroxyl groups, by optionally  
substituted phenyl groups, or by directly or indirectly  
attached polymer forming or biotargeting groups, eg.  
polyaminoacids, dendrimeric polymers, polyalkylene oxide  
groups, antibodies, antibody fragments, drugs, site  
specific peptidic groups (eg. oligopeptide binding  
motifs), etc.

Particular examples of appropriate ligands include  
DTPA, DTPA-BMA, DOTA, DO3A, HP-DO3A, BOPTA, PAMAM-  
polyDTPA, and PAMAM-polyDOTA. Especially preferred  
ligands include DTPA, DTPA-BMA, DOTA, and HP-DO3A.

The metallation reaction is preferably performed in  
aqueous solution, eg. in distilled water optionally  
containing a miscible cosolvent, at an elevated  
temperature, eg. 70 to 95°C, preferably 80-90°C. During  
the reaction the pH is preferably 3 to 6. The pH may be  
controlled by addition of an acid or base, preferably an  
acid or base which produces pharmaceutically acceptable  
neutralisation products, such as hydrochloric acid and  
sodium hydroxide.

The progress of the metallation reaction will  
generally be monitored to determine the residual  
quantities of unreacted lanthanide oxide or ligand, with  
extra portions of oxide or ligand optionally being added  
until the reaction is deemed to be complete, eg. when a

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stable low concentration of ligand and negligible free lanthanide is detected. The reaction mixture will then be cooled, eg. to below 25°C. If necessary the pH of the reaction mixture is then adjusted, eg. about 6, for example using sodium hydroxide. The solution is then filtered and the lanthanide complex is isolated, eg. by crystallisation.

Using this procedure, the metallation reaction time for a ligand such as DTPA-BMA may be reduced from 2 to 3 hours to 1 hour or below, eg. 30 minutes.

Viewed from a further aspect the invention provides the use of oxalic acid (or a salt or derivative thereof) and/or a lanthanide oxide having a oxalate content of at least 100 µg oxalic acid /g lanthanide oxide, preferably at least 200 µg/g, as a reaction accelerator in the lanthanide metallation of a ligand.

The invention will now be described further with reference to the following non-limiting Examples.

#### EXAMPLE 1

A reactor vessel is charged with 180 mL of distilled water. After cooling to below 50°C, 43.2 g (119.17mmoles) gadolinium oxide and 30.2 mg oxalic acid dihydrate are added. (The oxalic acid represents 500 ppm relative to the gadolinium oxide). During stirring, 100 g (238.42 mmoles) DTPA-BMA is added in one portion and the mixture is heated to 80-90°C. After 0.5 hours, a sample of the reaction mixture is taken and analysed for the content of unreacted DTPA-BMA. If DTPA-BMA content is below 1% (w/v) a new sample is taken and analysed to confirm that the DTPA-BMA content is low and stable. If the DTPA-BMA content is above 1% w/v, the reaction mixture is stirred until sampling and analysis shows DTPA-BMA content to have stabilized below 1% w/w. (Optionally further DTPA-BMA or gadolinium oxide may be added to complete the reaction).



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After complexation is complete, the reaction mixture is cooled to below 25°C. If necessary the pH is adjusted to about 6.1 to 6.4 by the addition of aqueous sodium hydroxide. The solution is filtered and GdDTPA-BMA is crystallized out.

#### EXAMPLE 2

An oxalate-contaminated batch of gadolinium oxide was analysed for oxalic acid content by titration with potassium permanganate in sulphuric acid. The content was found to be 270 µg oxalic acid per gram Gd<sub>2</sub>O<sub>3</sub>.

A sample of this batch was heated to 1100°C for 2 hours to decompose the oxalate contamination.

Three metallation reactions were carried out using (i) heat treated contaminated gadolinium oxide, (ii) contaminated gadolinium oxide and (iii) contaminated gadolinium oxide with the further addition of 230 µg/g Gd<sub>2</sub>O<sub>3</sub> of oxalic acid. The ligand was DTPA-BMA and the metallation reaction was carried out in aqueous solution at 80°C. The times required for the reactions to go to completion were respectively 2.5 hours, 1 hour and less than ½ hour.

Claims

1. A process for the preparation of a lanthanide complex by reaction of a lanthanide oxide with a complexing agent in an aqueous reaction medium, characterised in that oxalic acid or a salt or derivative thereof is used as a reaction accelerator.
2. A process as claimed in claim 1 wherein said lanthanide is gadolinium.
3. A process as claimed in either of claims 1 and 2 wherein oxalic acid is used as the reaction accelerator.
4. A process as claimed in any one of claims 1 to 3 wherein 200 to 1000  $\mu\text{g}$  oxalic acid/g lanthanide oxide are used as the reaction accelerator.
5. A process for the preparation of a lanthanide complex by reaction of a lanthanide oxide with a complexing agent in an aqueous reaction medium, characterised in that said process comprises the steps of: (a) determining the level of impurity in the lanthanide oxide; and (b) mixing a lanthanide oxide from batches with different determined levels of impurity and/or including in the reaction medium a predetermined quantity of oxalic acid or a salt or derivative thereof; whereby by virtue of step (b) the reagents used in the metallation reaction contain oxalic acid (or salt or derivative) or oxalate at a total level of at least 50  $\mu\text{g}$  oxalic acid per gram lanthanide oxide.
6. A process as claimed in claim 5 wherein said lanthanide is gadolinium.
7. A process as claimed in either one of claims 5 and 6 wherein a predetermined amount of oxalic acid or a salt or derivative thereof is included in the reaction

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medium.

8. A process as claimed in claim 7 wherein a predetermined amount of oxalic acid is included in the reaction medium.

9. A process for the preparation of a lanthanide complex by reaction of a lanthanide oxide with a complexing agent in an aqueous reaction medium, characterised in that for use as said lanthanide oxide is selected a lanthanide oxide having an oxalate impurity level of at least 100  $\mu\text{g}$  oxalic acid/g lanthanide oxide.

10. A process as claimed in claim 9 wherein said lanthanide is gadolinium.

11. A process as claimed in any one of claims 1 to 10 wherein said complexing agent is a polyaminopoly-carboxylic acid.

12. A process as claimed in claim 11 wherein said complexing agent is selected from DTPA, DTPA-BMA and HP-DO3A.

13. A process as claimed in claim 11 wherein said complexing agent is DTPA-BMA.

14. The use of oxalic acid and/or a lanthanide oxide having a oxalate content of at least 100  $\mu\text{g}$  oxalic acid/g lanthanide oxide, as a reaction accelerator in the lanthanide metallation of a ligand.

# INTERNATIONAL SEARCH REPORT

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A. CLASSIFICATION OF SUBJECT MATTER  
IPC 6 C07C227/18

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC-6 C07C C07F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US 4 647 447 A (GRIES HEINZ ET AL) 3 March 1987 cited in the application -----	1

☐ Further documents are listed in the continuation of box C.

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